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(54) **Batch liquid purifier**

(57) A batch liquid purifier (10) using a reservoir
(11), an ozone generator (15), and a pumping system
(20) is arranged for contacting the liquid with an ozone
containing gas so that it is purified either during a direct
outflow to a purified liquid chamber (12) or during a cir-

culational flow back to a reservoir. The flow circuit can
include a liquid gas separator (21) and venting of gas to
atmosphere via an ozone concentration reducer (23).
Pumping, valving, and controls can be accomplished in
a variety of ways, as illustrated for systems.

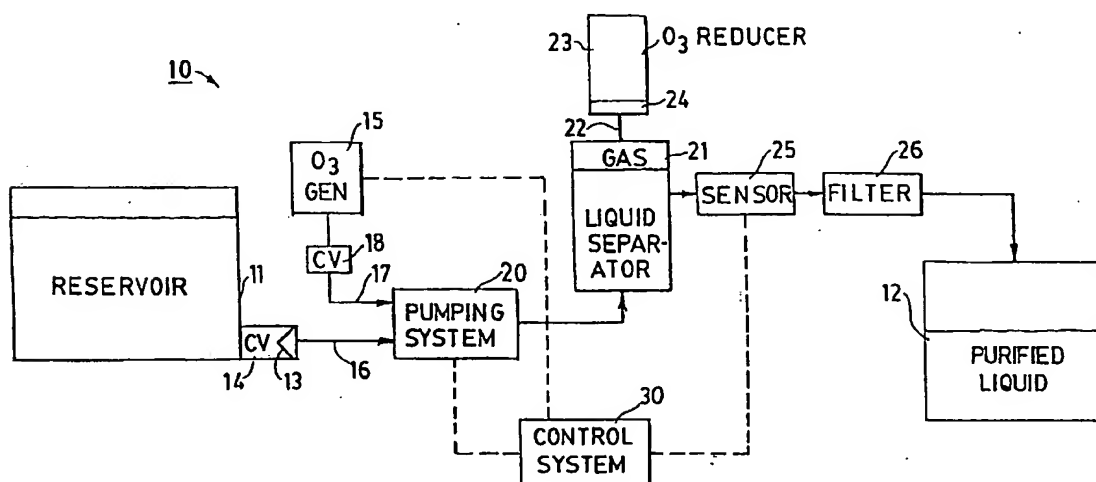


FIG. 1

Description

TECHNICAL FIELD

This invention involves ozone purification of batches of liquid with equipment made small enough to operate on a countertop or in space available below a counter.

BACKGROUND

By this invention, I have reduced the size, complexity, and expense of equipment for purifying batches of liquid with ozone; and by carefully selecting and combining components, I have been able to make smaller scale ozone purification equipment operate conveniently and reliably for safely purifying liquid batches within reasonably short times. Equipment according to my invention can be operated on a residential countertop or in a small space under a counter, for example, to produce purified liquid batches less than 20 liters in size.

SUMMARY OF THE INVENTION

The purifier of this invention includes a generator that makes an ozone containing gas and operates on a batch basis with a reservoir or chamber sized for holding less than 20 liters of liquid. By one arrangement, the liquid flows through a passageway from the reservoir to a purified liquid container, and a gas passageway from the generator leads ozone to the liquid passageway. A pumping system causes the liquid to flow through the liquid passageway and causes the gas to contact the liquid with ozone to effect its purification as it proceeds toward the purified liquid container. The pumping rate and the dimensions of the liquid and gas passageways determine the flow rates of the liquid and the ozone containing gas. In a recirculating arrangement, the liquid flows through a liquid passageway leading back to the reservoir, and a pumping system is arranged for flowing the liquid into contact with the ozone containing gas in a circulatory path during purification. A pumping system can also be arranged for contacting the liquid with ozone containing gas during a purification cycle, and then outputting purified liquid during an output cycle.

DRAWINGS

All of the drawings are partially schematic diagrams of different preferred embodiments of my batch liquid purifier. Each embodiment includes an ozone generator, a reservoir of liquid to be purified, a pumping system for bringing ozone into contact with the liquid to be purified, a reducer for diminishing the concentration of any escaping ozone, and a controller to ensure that liquid purification occurs. The various embodiments of the drawings differ from each other in that:

Figure 1 shows an in-line system for pumping liquid

from a reservoir to a purified liquid container while contacting the liquid with ozone to ensure its purification.

Figures 2-4 schematically show three preferred alternatives for pumping systems usable in the embodiments of FIGS. 1 and 5-9.

Figure 5 schematically shows a bypass system that can purify liquid while it is pumped through a circulatory path from and back to a reservoir, with an alternate route leading to an outlet.

Figure 6 shows a pump, valve, and control system usable for the pumping system of FIG. 5.

Figure 7 shows another bypass and alternative output system, similar to the system of FIG. 5, but differing in the pumping and valving arrangement.

Figure 8 shows another bypass system having a purified liquid output from the liquid reservoir.

Figure 9 shows a system using two pumps, one for pumping ozone into a reservoir for purifying liquid and another for pumping purified liquid to an outlet.

DETAILED DESCRIPTION

The preferred embodiments of the drawings have comparative advantages in features such as convenience, reliability, safety, cost, and compactness. Different embodiments, using different combinations of such features, may be preferred for different users with different desires. The embodiments will be explained in the order presented in the drawings, but this does not imply any similar order of importance. Also, some of the different features that are illustrated in the drawings can be interchanged among the various embodiments, and the drawings are arranged to illustrate the different features that can be combined, and not to delimit one combination of features from another.

The reasons that the purifier embodiments can be varied so extensively include the many different uses for liquid purifiers and the correspondingly different considerations for expense, space requirements, and batch size. One important use is purifying water for drinking and cooking purposes. This can be done on or below a countertop with batches sized for coffeepots and hand-held pitchers. Different users will require different levels of sophistication in convenience and extent of automatic performance. Water can also be purified on a batch basis for small scale requirements in laboratories, offices, and industries. The liquid to be purified is not necessarily water, and my purifiers can be applied to purifying saline solution, for example. This could be desirable in an optometrist's office, for rinsing and storing contact lenses.

The liquid purifier 10 of FIG. 1 purifies raw liquid as it flows from reservoir 11 to purified liquid container 12. A pumping system 20 directs the liquid flow from reservoir 11 to container 12 and contacts the liquid with an ozone containing gas from generator 15 so that the liquid is purified as the flow occurs.

Reservoir 11 and container 12 are sized to hold less than 20 liters of liquid and can be made small enough

to hold one coffee pot full of liquid, for example. Reservoir 11 can have a quickly releasable connection 13 that includes a check valve 14 for connecting and disconnecting reservoir 11 with liquid flow line 16 leading to pumping system 20. A gas flow line 17 leads from ozone generator 15, preferably via a check valve 18, to convey a gas and ozone mixture to pumping system 20. Besides conventional check valving, check valve 18 can be formed of a porous hydrophobic material that allows gas to pass through but prevents any liquid backflow from reaching generator 15. This is especially desirable when generator 15 is the preferred corona discharge generator that would be damaged by presence of any liquid. Suitable porous hydrophobic materials can include hydrophobic resin or plastic materials that are made porous to allow passage of gas, but block the passage of liquid. Porous inorganic materials may also be usable for this. The entire material does not need to be hydrophobic, so long as a hydrophobic material is arranged to serve as a liquid barrier combined with an otherwise porous material. These considerations also apply to other uses of porous hydrophobic materials in my purifiers, as explained below.

Although ambient air is a simple and preferred input for generator 15, it is also possible to use dried air that has passed through a dryer to help keep moisture out of generator 15. Another possibility is supplying oxygen from a small container serving as the input to generator 15, which can produce more ozone from an oxygen supply than from an air supply.

Pumping system 20 can take several forms, as explained more fully below. Generally, it draws liquid from reservoir 11 via liquid line 16 and contacts the liquid with ozone contained in a gas drawn via line 17 so that the ozone purifies the liquid before it reaches chamber 12. In the embodiment of FIG. 1, the gas and liquid output from pumping system 20 is directed to a gas and liquid separator 21. The gas drawn from generator 15 and combined with the liquid by pumping system 20 separates from the liquid in separator 21 and is vented to atmosphere. This preferably occurs through an ozone reducer 23 that reduces the concentration of ozone in any gas entering the atmosphere. Reducer 23 contains at least one of several materials that are available for reducing the ozone concentration or changing the ozone into ordinary oxygen so that raw ozone does not escape into the atmosphere. Even if raw ozone were to escape through vent 22, however, it should not present any health hazard in the small quantities used for operating system 10.

There are several ways that gas and liquid separator 21 can operate. The liquid level is preferably controlled by a float valve, which has the advantage of keeping the liquid pressurized. Gravity can also be used to provide a liquid surface above which gas can rise. Another possibility is to arrange a porous hydrophobic element to form a barrier for liquid, while allowing gas to pass. The liquid and gas separation can occur separate from

a liquid reservoir or purified liquid storage, or can be combined with these, as explained below.

When reducer 23 is used and is filled with a catalytic or reactive material that reduces the ozone concentration or changes the ozone into oxygen, it is important that liquid not reach the material within reducer 23, because liquid would impair its action. Working against this is the fact that gas bubbles enter separator 21 and burst at the liquid surface there, creating spray droplets that can enter vent 22. Baffles are one possibility for keeping these spray droplets out of reducer 23, but baffles would not block liquid flow if the system were overturned. What I prefer, therefore, is a porous hydrophobic element 24 that allows gas, but not liquid, to enter reducer 23.

From gas and liquid separator 21, liquid proceeds to purified liquid container 12. In doing so, purified liquid can flow past sensor 25, to detect the concentration of dissolved ozone in the liquid to verify that the liquid is adequately purified. Sensor 25 is preferably in communication with control system 30, which operates pumping system 20 and ozone generator 15. Control system 30 preferably includes a timer for timing each operation of system 10. An ozone sensor can also be arranged in this and other embodiments of my purifiers to ensure that purified liquid output does not contain more than a minimum of dissolved ozone. A timer can also be involved with control system 30 to ensure adequate deoxygenation of purified liquid output. Ozone sensors and timers for this purpose are preferably arranged in communication with the purified liquid storage or purified liquid output flow.

The flow of purified liquid into chamber 12 can also pass through filter 26, which can contain activated carbon or a catalyst that greatly reduces the concentration of dissolved ozone remaining in the purified liquid. This can be advantageous in situations requiring that little or no dissolved ozone remain in the liquid that is output from chamber 12. Other ways of ensuring this are to let the purified liquid stand for a few minutes in chamber 12 before using it, to aerate the purified liquid before using it, or to subject the purified liquid to ultraviolet light. By whatever method is used, the dissolved ozone concentration should be reduced before the purified liquid is output for use or consumption. For most purposes, dissolved ozone is acceptable in the purified liquid; and no health hazard has yet been identified with directly consuming water containing dissolved ozone at levels found in system 10.

Control system 30 also preferably includes a switch that initiates operation of system 10. This can run pumping system 20 and ozone generator 15 for long enough to empty reservoir 11 and transfer purified liquid to chamber 12. Sensor 25 can verify from the presence of dissolved ozone in the passing liquid that ozone generator 15 is operating and delivering ozone to the moving liquid. If sensor 25 does not detect ozone in the liquid, a warning or indicator light could be illuminated to inform the operator, or control system 30 could shut down

pumping system 20 and generator 15.

Several alternative pumping systems 20, suitable for use in system 10 of FIG. 1, are shown in FIGS. 2-4. These pumping systems can also be used in other preferred embodiments of my liquid purifier. The flow rates of liquid and gas through any pumping system used with my liquid purifier are preferably adjusted by sizing the liquid and gas conduits relative to the pumping rate and the force causing flow to occur. This eliminates the expense of detecting and metering flow rates to ensure adequate contact of liquid with ozone. The time that liquid and ozone are in contact with each other is also a factor in the purification process, since purification is a function of both the extent and the duration of ozone contact with liquid. Thus, pumping systems and liquid and gas flow lines should be selected to ensure proper flow rates of liquid and gas and adequate contact times between liquid and the ozone contained in the gas.

The pump 27 of FIG. 2 is preferably a positive displacement pump that receives the combined flows of liquid in line 16 and an ozone containing gas in line 17. Pump 27 then mixes and contacts the gas and liquid so that within pump 27 and downstream of pump 27, the liquid is in purifying contact with ozone. I have found that positive displacement pumps are good at mixing liquid and gas for contact purposes, but other types of pumps can also be used. Moreover, it is possible to use a static mixer 28 downstream of pump 27, to increase the mixing action.

Pump 31 of the embodiment of FIG. 3 is also a liquid pump and can move liquid by positive displacement or by some other pumping means. Downstream of pump 31 is a venturi 32 that draws in an ozone containing gas from line 17 to mix with and contact the liquid flowing from pump 31.

Pump 33, of the embodiment of FIG. 4, is a gas pump that forces the ozone containing gas through line 17 into chamber 34 from which a bubble line 35 extends. Gas bubbles rising in chamber 34 not only contact liquid present there, but also pump the liquid through bubble line 35 as the bubbles rise. This moves the gas and liquid mixture downstream toward gas and liquid separator 21 (not shown in FIG. 4).

Gas pump 33 is preferably arranged upstream of generator 15 so that it can force gas through generator 15, which outputs a mixture of gas and ozone. Pump 33 can also be arranged downstream of ozone generator 15, except that an ozone environment is too corrosive and problematic for most pumps to handle. Although pumping system 20 is shown in FIGS. 1 and 5-9 as downstream of generator 15, when a pumping arrangement such as shown in FIG. 4 is used for a pumping system 20, gas pump 33 is preferably arranged upstream of generator 15.

System 35, as shown in FIG. 5, uses a circulation loop to draw liquid from reservoir 36 and return liquid back to reservoir 36 while purification occurs during a circulatory flow. Reservoir 36 then serves also as the

purified liquid container and as the gas and liquid separator. Any ozone flowing out of reservoir 36 via vent 22 passes through ozone reducer 23, which is preferably protected by a porous hydrophobic element 24, as explained above. Reservoir 36 can be filled via a trap 37 and can have a drain 38. Sensor 25 can be located in reservoir 36 to detect the presence of dissolved ozone and communicate this to control system 30. A switch 58 can initiate a purifying operation of system 35, and control system 30 preferably includes a timer arranged for operating system 35 for a minimum duration. Output of purified liquid is preferably initiated in response to switch 39.

A filter 40 can be arranged in line 16 for liquid outflowing from reservoir 36; and in such a position, filter 40 accomplishes some liquid filtration both before and after contact with ozone, because of the circulatory flow. Flowing the contents of reservoir 36 three or four times through the circulatory loop that includes pumping system 20 and filter 40 is generally enough to complete the purification of the liquid. Passage through filter 40 before liquid is contacted with ozone can remove some impurities and reduce the purification load required of the ozone treatment. Passage of liquid through filter 40 after contact with ozone can remove materials precipitated by the ozone contact.

After a purifying circulation, liquid can be output from reservoir 36 by changing the route through pumping system 20 so that instead of flowing back into reservoir 36 via line 41, liquid flows to an outlet from pumping system 20. This can lead through filter 42, which can remove precipitated materials and which can reduce the concentration of any ozone still dissolved in the liquid, before the purified liquid is output from the purifier.

There are several ways that pumping system 20 can be arranged to accomplish both the purified liquid outflow and a circulatory flow during purification, and one of these is shown in FIG. 6. Liquid pump 43 can pump a liquid flow to valve 44 under control of control system 30 so that during circulatory flow, valve 44 directs liquid flow through venturi 45, which draws in an ozone and gas mixture and contacts it with flowing liquid on the way back to reservoir 36 through line 41. When purification is completed and outflow is desired, valve 44 changes state, preferably in response to an outflow switch so that liquid flows directly to an outlet from pump 43. Generator 15 is preferably turned off while this occurs.

System 50, as shown in FIG. 7, is similar to system 35 in circulating liquid flow from and to reservoir 36. It differs in using a gas and liquid separator 21 with an ozone reducer 23 and vent 22, as explained above, and using a manually operated valve 46. This directs flow back to reservoir 36 through line 41 during purification and directs purified liquid to an outlet via filter 42. Filter 40 can be arranged in line 41 to help remove impurities during the purification flow; or, alternatively, filter 40 can be arranged in line 16 upstream of line 17 from ozone generator 15. Pump 47 is preferably a positive displacement

ment liquid pump that pumps a gas and liquid mixture to separator 21. Control system 30 preferably includes a switch and timer and can communicate with sensor 25 in reservoir 36, as previously explained. Valve 46 is preferably arranged in communication with control system 30 so that when valve 46 is manually operated to deliver an outflow, only pump 47 is turned on, without energizing ozone generator 15. Liquid can also be output from system 50 by using a momentary electric switch that simultaneously operates pump 47 and electrically positions valve 46 to deliver an outflow.

System 55 of FIG. 8 also operates a circulatory flow from and to reservoir 36 via gas and liquid separator 21, but uses pumping system 20 only to power the circulatory flow during purification, and not to power the output flow. The outflow of purified liquid from reservoir 36 is via valve 48, which can be manually operated, and which uses a gravity powered outflow. Filter 40 can be arranged in the circulatory loop to remove impurities from the liquid, and pumping system 20 can have any of the forms described above in FIGS. 2-4. Operation is controlled by system 30, which can communicate with sensor 25 in reservoir 36 to ensure that liquid is adequately purified.

Two pumps are used in system 60 of FIG. 9. A gas pump 51 pumps an oxygen-containing gas such as ambient air, dried air, or oxygen into ozone generator 15 so that an output gas containing ozone is bubbled through diffuser 52 into the liquid in reservoir 36. The bubbles contact the liquid with ozone and accomplish its purification within reservoir 36. Diffuser 52 is porous and allows gas to flow through, preferably in a way that divides the gas flow into a multitude of bubbles. Although air stones and other materials are available for diffuser 52, I prefer a porous element made from or including a hydrophobic material that allows the ozone containing gas to flow through, but resists any flow of liquid in the opposite direction. Since a multitude of small bubbles are desirable for liquid-gas contact, and since a bubble diffuser of a given pore size produces smaller bubbles if the surface tension of the diffuser material is increased, there may be advantages in using separate materials to provide the porous hydrophobic liquid barrier and a porous bubble diffuser. For example, a hydrophilic porous material or coating on top of a porous hydrophobic material can exploit the advantages of both materials. There are also many different ways of combining porous hydrophobic liquid barriers and other porous materials producing fine diffused bubbles.

By including a porous hydrophobic material, diffuser 52 can then serve as a liquid barrier, ensuring that no liquid travels back to generator 15. This is important because the preferred form of generator 15 is a corona discharge device that would be damaged if liquid were to enter it. Trap 37, also suggested for the embodiment of FIG. 5, is preferred for adding liquid to reservoir 36.

Another way to ensure that liquid does not enter generator 15 is by directing the output from generator

15 to a level higher than the liquid level within the system so that gravity prevents liquid from flowing through the elevated passageway to generator 15. This would require that the system not be turned over while it contains liquid. A check valve can also be arranged in output line 17 from generator 15, as shown in some of the other embodiments, to help protect generator 15 from liquid.

Reservoir 36 also serves as a gas and liquid separator, allowing gas to flow through vent 22 and ozone reducer 23, which is preferably protected from liquid by porous hydrophobic element 24. Sensor 25 can detect the presence of dissolved ozone in the liquid in reservoir 36 so that control system 30 can operate the purification cycle long enough to ensure that the liquid is adequately purified.

Liquid pump 53 outputs purified liquid from reservoir 36, preferably in response to a demand switch 54 arranged near the outlet and communicating with control system 30. The purified liquid outflow through pump 53 can also pass through filter 56 to remove any precipitated impurities and to reduce the concentration of any ozone still dissolved in the purified liquid, before the liquid is output.

System 60 can be operated, by actuation of switch 58, to purify a liquid batch in reservoir 36 and then in response to switch 54 to flow the purified liquid to the outlet on demand. Reservoir 36 can be refilled on a batch basis preferably via trap 37 or from a pressurized supply line via a valve that is not shown in FIG. 9. It can also have a drain 57 and can be arranged under a countertop or in a basement below a kitchen, for example, since pump 53 allows it to deliver the outflow to a higher elevation.

Claims

1. A batch operation purifier using a generator that makes an ozone containing gas, said purifier comprising:
 - a. a reservoir sized for holding less than 20 liters of a liquid;
 - b. a liquid passageway arranged for conducting said liquid from said reservoir to a junction;
 - c. a gas passageway arranged for conducting said ozone containing gas from said generator to said junction, where said ozone containing gas contacts said liquid;
 - d. a contact passageway arranged downstream of said junction where said liquid and said ozone containing gas can flow in contact with each other, said contact passageway being arranged for conducting said liquid back to said reservoir;
 - e. a pumping system arranged for flowing said liquid through said liquid passageway to said junction, flowing said ozone containing gas

- through said gas passageway to said junction,
and flowing a mixture of said liquid and said
ozone containing gas from said junction into
said contact passageway and at least said liq- 5
uid back to said reservoir so that circulation of
said liquid contacts said liquid with said ozone
sufficiently to purify said liquid in said reservoir;
f. said pumping system and said liquid and gas
passageways being sized to determine the flow 10
rates of said liquid and said ozone containing
gas through said passageways; and
g. means for reducing the concentration of any
ozone escaping into the atmosphere.
2. The purifier of claim 1 wherein said pumping system 15
includes a pump arranged so that said pump con-
tacts said ozone containing gas with said liquid by
mixing.
 3. The purifier of claim 1 or claim 2 including a sepa- 20
ration chamber arranged in said contact passage-
way for separating said ozone-containing gas from
said liquid after they have been contacted but be-
fore the said liquid is returned to said reservoir. 25
 4. The purifier of any one of the preceding claims in-
cluding a contact chamber downstream of said
junction where said ozone-containing gas is bub-
bled through said liquid. 30
 5. The purifier of any one of the preceding claims in-
cluding a sensor arranged for sensing the concen-
tration of ozone in the liquid.
 6. The purifier of claim 5 including a control system 35
responsive to said sensor for controlling the opera-
tion of the purifier.
 7. The purifier of any one of the preceding claims
wherein the pumping system includes a pump in the 40
liquid passageway and the junction is a Venturi
downstream of the said pump.
 8. The purifier of any one of the preceding claims 45
wherein the pumping system is operable to pump
liquid out of the reservoir to an outlet from the puri-
fier.
 9. The purifier of claim 8 including means for reducing 50
the concentration of ozone dissolved in said liquid
in said reservoir before dispensing liquid from the
outlet from the purifier.
 10. The purifier of any one of the preceding claims in- 55
cluding a device making said reservoir connectable
to and disconnectable from said liquid passageway
without loss of liquid.

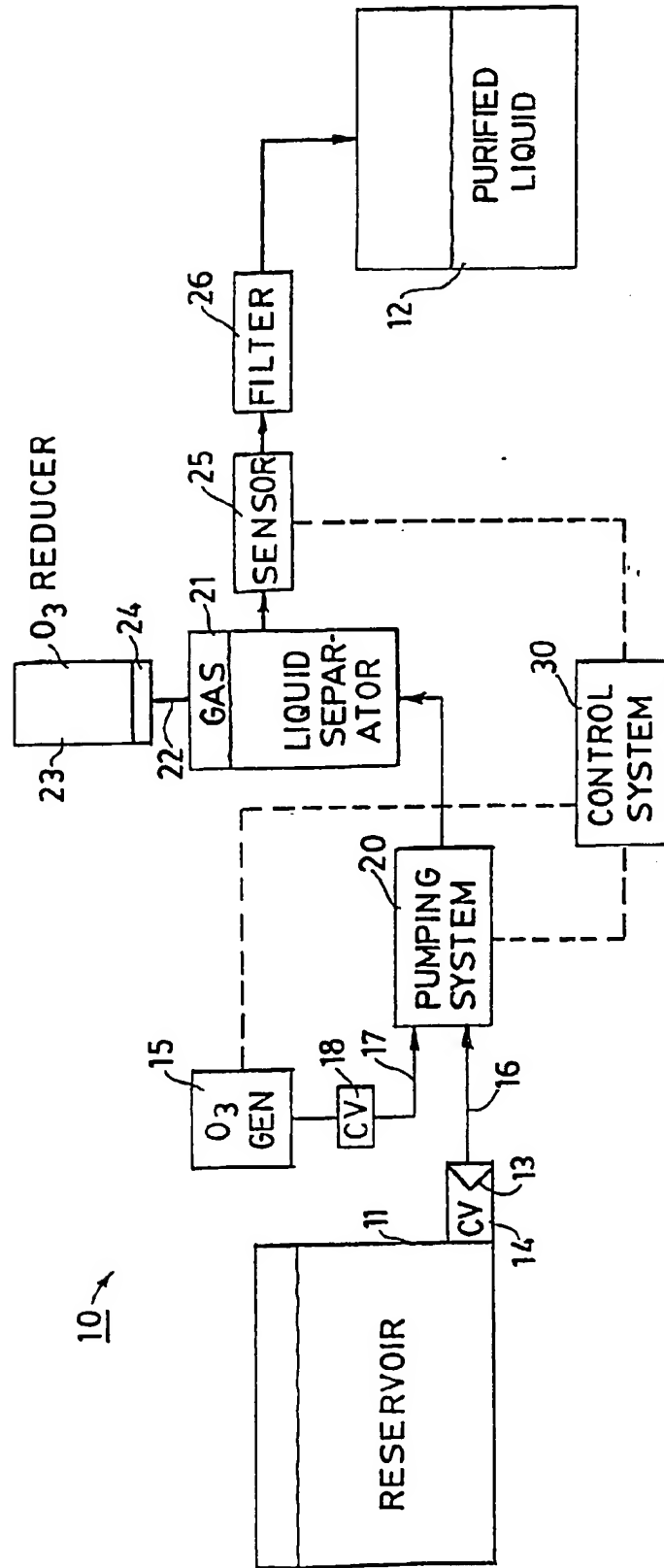
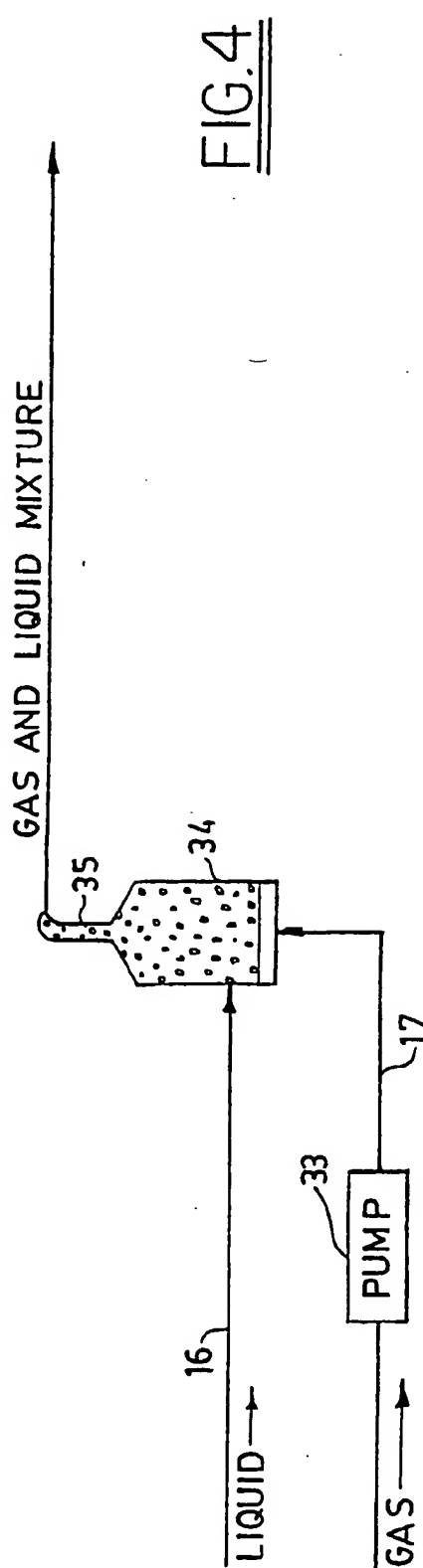
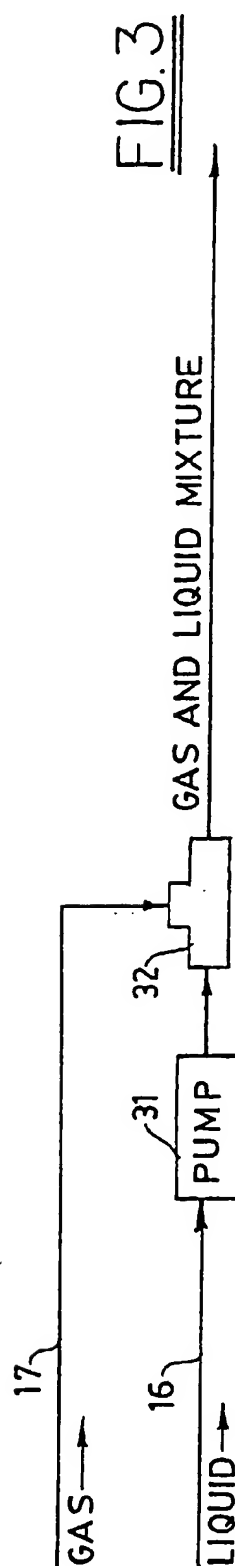
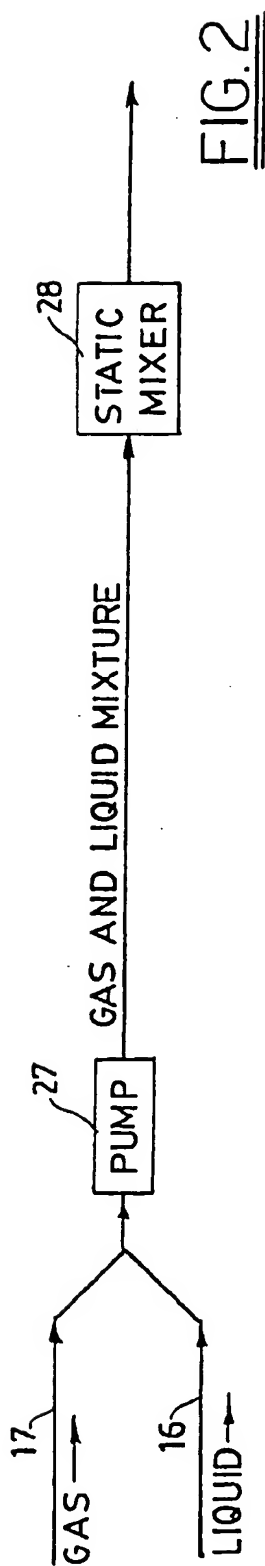
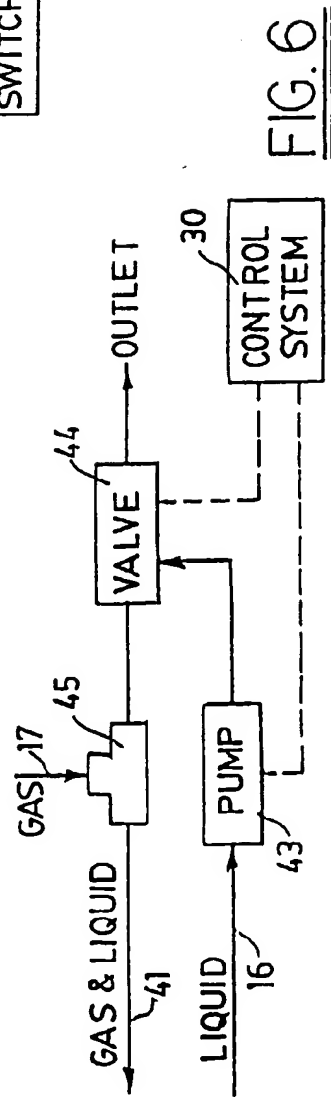
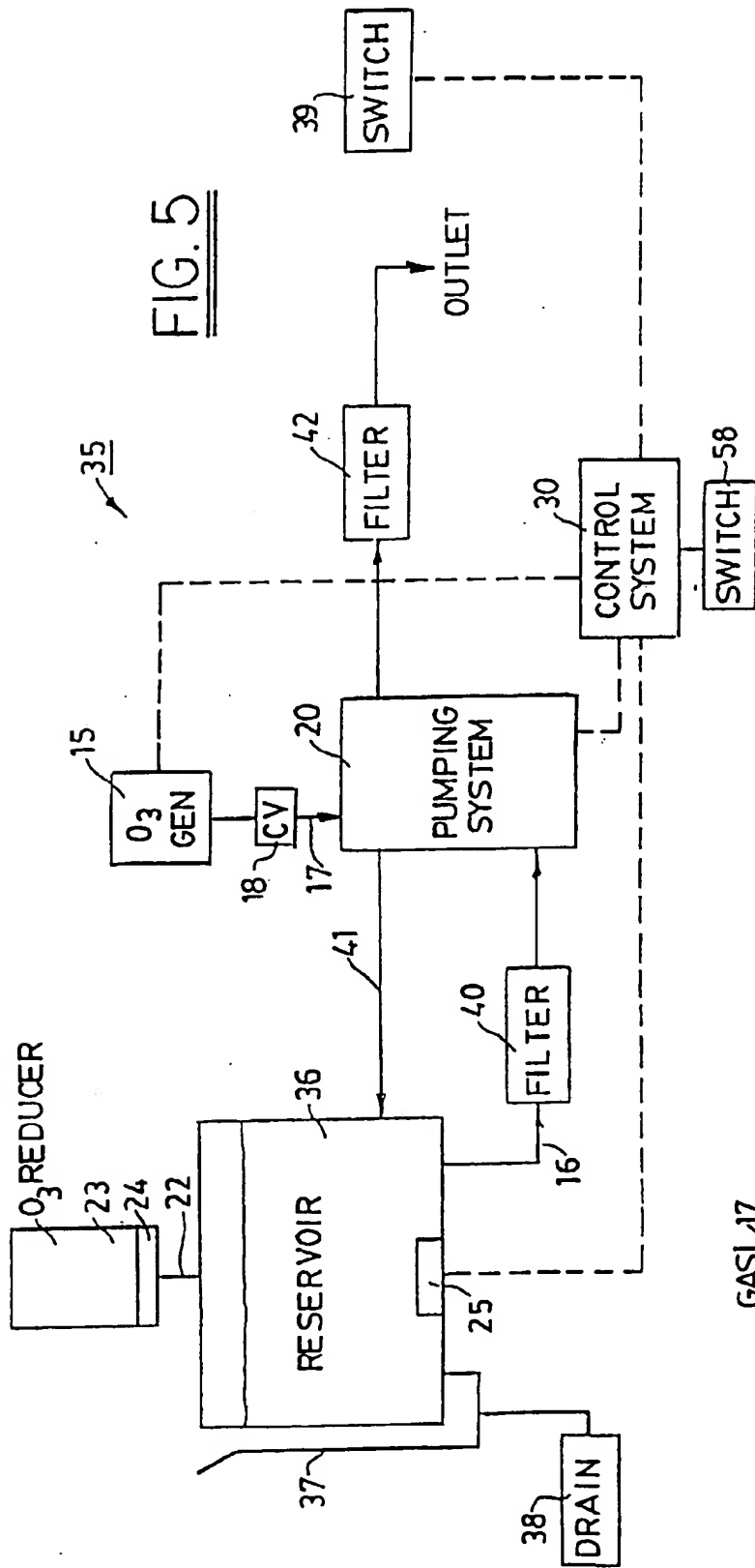


FIG.1





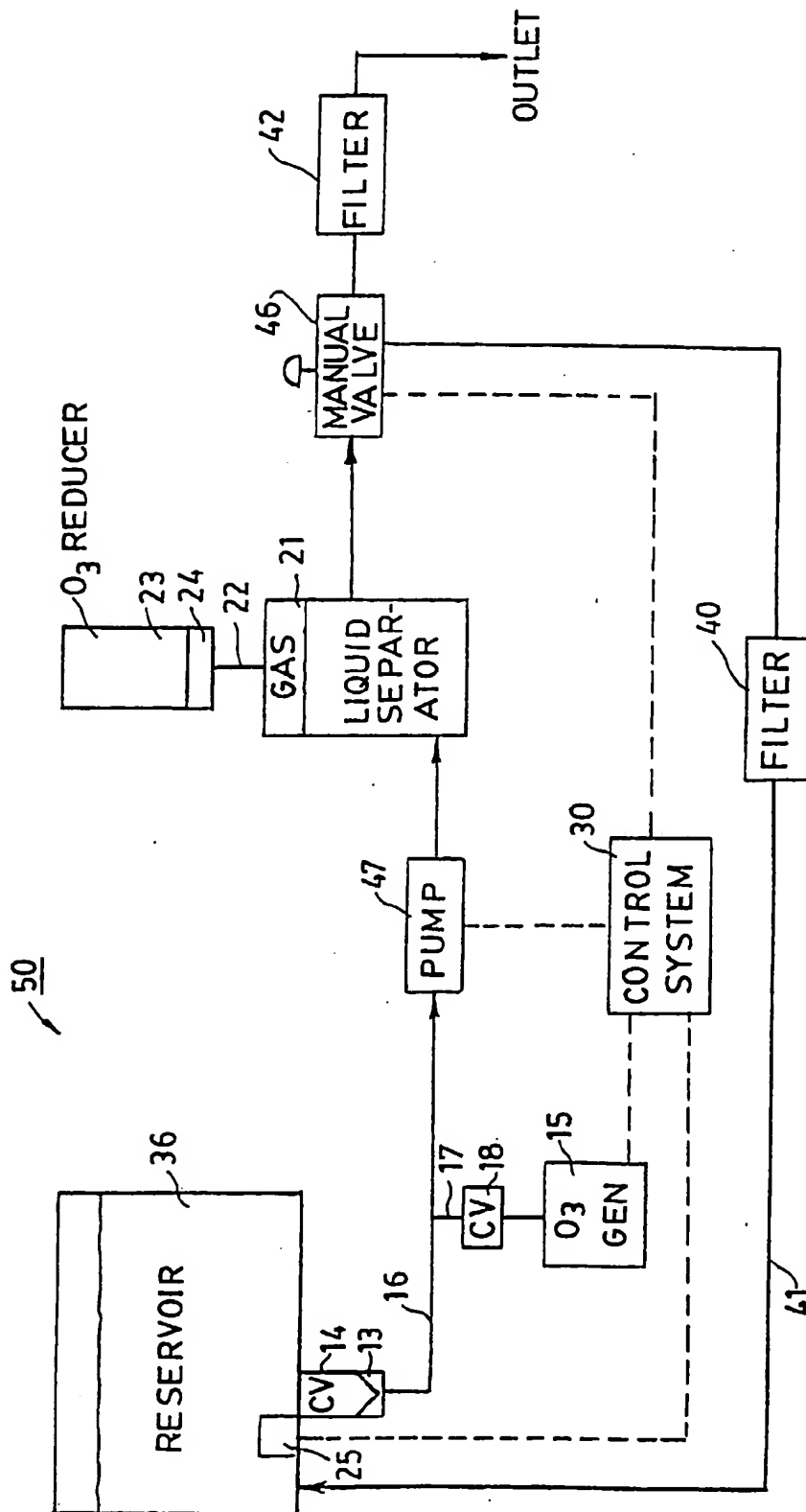
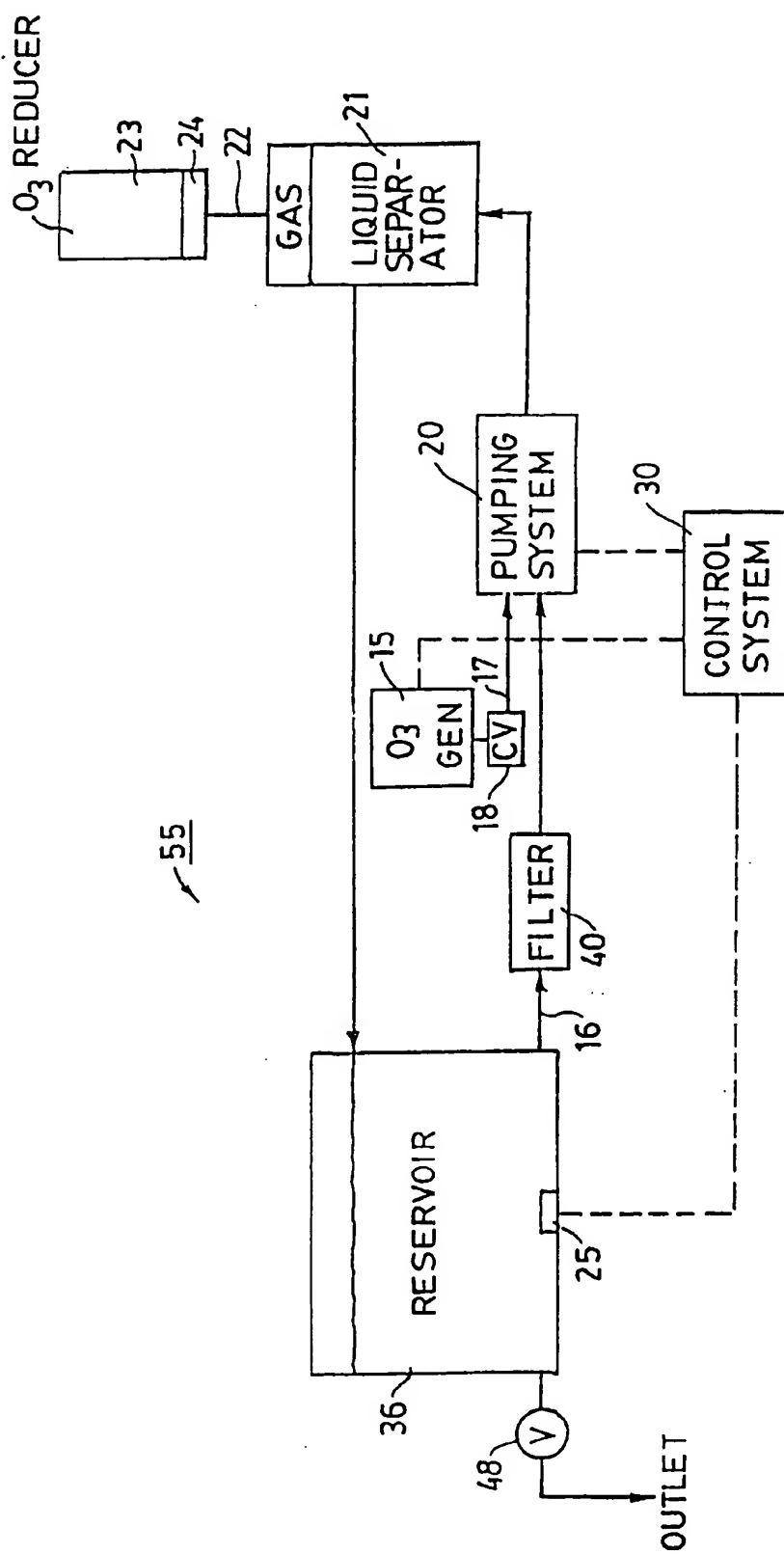


FIG. 7



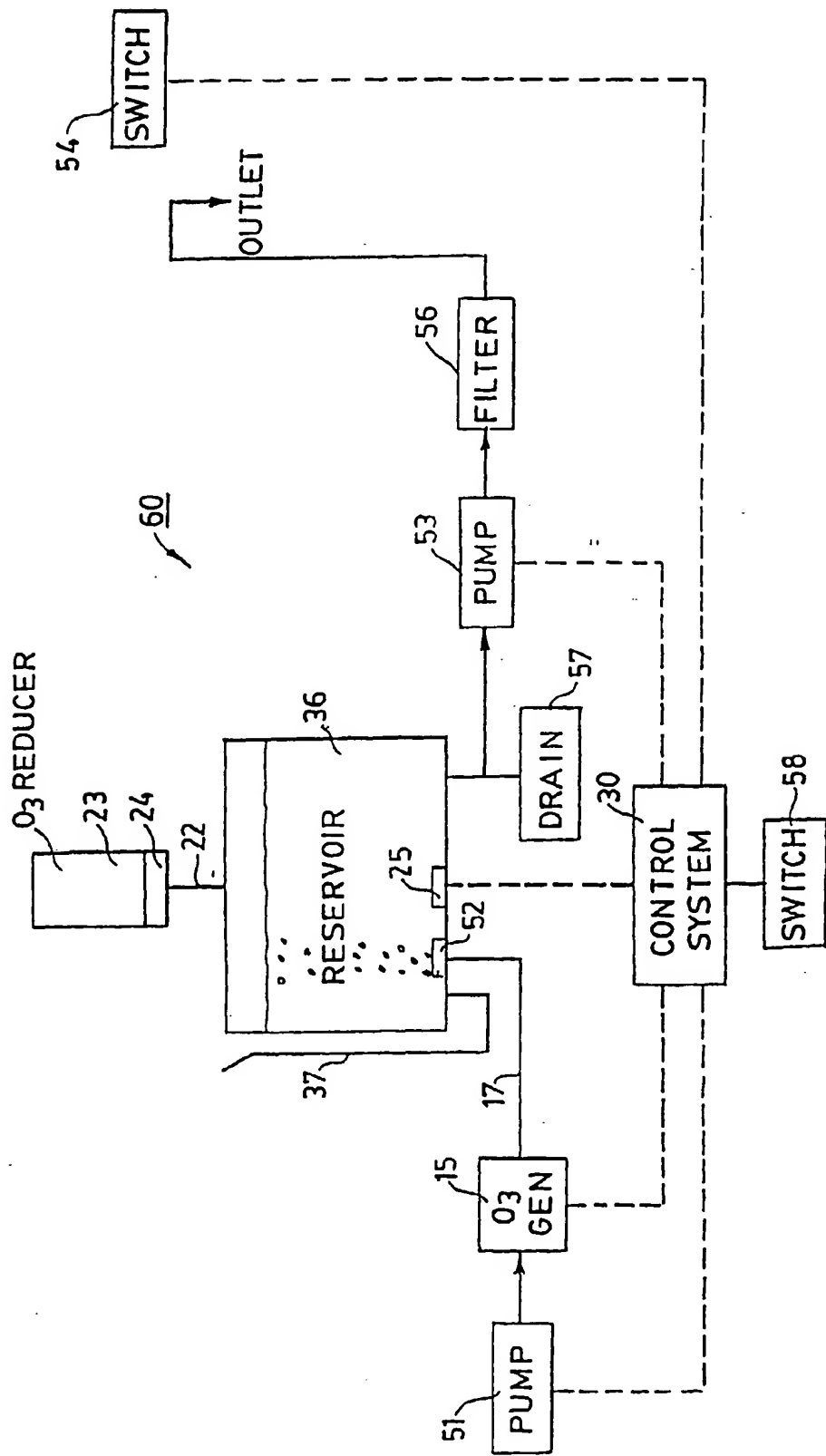


FIG. 9



European Patent
Office

EUROPEAN SEARCH REPORT

Application Number
EP 98 11 6912

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.6)
P, A	US 5 082 558 A (BURRIS) 21 January 1992 * the whole document * ---	1-10	A61L2/00 B01D19/00 B01J19/08 C02F1/78
A	US 4 599 166 A (GESSLAUER) 8 July 1986 * the whole document * ---	1-10	
A	US 4 298 467 A (GARTNER ET AL) 3 November 1981 * claims; figure 5 * ---	1-10	
A	US 3 823 728 A (BURRIS) 16 July 1974 ---		
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The present search report has been drawn up for all claims			TECHNICAL FIELDS SEARCHED (Int.Cl.6) C02F
Place of search THE HAGUE		Date of completion of the search 10 November 1998	Examiner Ruppert, G
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